



## Letter to the Editor

Oxidative dissolution of actinide oxides in H<sub>2</sub>O<sub>2</sub> containing aqueous solution – A preliminary studyReijo Pehrman<sup>a</sup>, Marcus Amme<sup>a,1</sup>, Olivia Roth<sup>b,\*</sup>, Ella Ekeröth<sup>b,2</sup>, Mats Jonsson<sup>b</sup><sup>a</sup>European Commission, Joint Research Centre, Institute for Transuranium Elements, Postfach 2340, 76125 Karlsruhe, Germany<sup>b</sup>KTH Chemical Science and Engineering, Nuclear Chemistry, Royal Institute of Technology, SE-100 44 Stockholm, Sweden

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## ABSTRACT

Oxidative dissolution of spent nuclear fuel is an important issue in the safety assessment of a future geological repository for spent nuclear fuel. Although UO<sub>2</sub> constitutes, in terms of mass, the majority of the spent fuel material, its main radiotoxicity is (after extended storage times) contained in actinides with half lives shorter than that of 238-uranium, such as isotopes of Np and Pu. Relatively little information is available on the dissolution behavior of Np and Pu in comparable environments. This work investigates the oxidative dissolution of NpO<sub>2</sub> and PuO<sub>2</sub> in non-complexing aqueous solutions containing H<sub>2</sub>O<sub>2</sub> and compares their behavior with that of UO<sub>2</sub>. We have found that oxidative dissolution takes place for all three actinides in the presence of H<sub>2</sub>O<sub>2</sub>. Based on the obtained dissolution rates, we would not expect the dissolution of the actinides to be congruent. Instead, in a system without complexing agent, the release rates of Np and Pu are expected to be lower than the U release rate.

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## 1. Introduction

The envisaged geological final disposal of highly radioactive waste demands an investigation of the behavior of the waste materials in geological environments over long time scales. In the event of groundwater intrusion, the release of most radionuclides from spent nuclear fuel will be controlled by the dissolution of the fuel matrix, which (for most fuels) mainly consists of UO<sub>2</sub> [1]. UO<sub>2</sub> has low solubility under the reducing conditions that prevail at the depth of a deep repository, whereas the matrix solubility is increased upon oxidation [2]. When spent fuel comes into contact with water, oxidizing radiolysis products will be formed and the potential for matrix dissolution could increase significantly [3].

Although UO<sub>2</sub> constitutes, in terms of mass, the majority of the spent fuel material, its main radiotoxicity is (after extended storage times) contained in actinides with half lives shorter than that of 238-uranium, such as isotopes of Np and Pu and the point has been raised that potential incongruent dissolution of these actinides may be regarded as a safety-relevant effect when assessing spent fuel behavior [4]. The behavior of uranium dioxide in contact with oxidizing water radiolysis products such as hydrogen peroxide has been extensively investigated in recent years [5] whereas

experiments aiming at understanding the radiolytic dissolution kinetics of the homogeneous phases NpO<sub>2</sub> and PuO<sub>2</sub> can not be found in the open literature.

Although Np and Pu are higher homologues of U in the actinide series, it seems improbable that they will display identical oxidation and dissolution kinetics. The consequence of such differences may result in an incongruent dissolution from the spent fuel matrix under radiolytic conditions and deserve attention. This is increasingly important when considering long term deposition of MOX fuel and UO<sub>2</sub>-fuel with higher burn-up.

Previous studies on UO<sub>2</sub> have shown that, in a system exposed to  $\alpha$ -radiation, H<sub>2</sub>O<sub>2</sub> is the major contributor to the oxidative dissolution [6]. This work investigates the kinetics of H<sub>2</sub>O<sub>2</sub> consumption in aqueous solutions containing NpO<sub>2</sub> and PuO<sub>2</sub> and compares their behavior with that of UO<sub>2</sub>.

## 2. Experimental

Experiments have been performed where the reaction between actinide oxides and H<sub>2</sub>O<sub>2</sub> were studied by mixing aqueous suspensions of AnO<sub>2</sub> powders with H<sub>2</sub>O<sub>2</sub> solutions and monitoring the H<sub>2</sub>O<sub>2</sub> concentration and the concentration of dissolved An versus time. Radionuclides used in this study are depleted uranium, <sup>237</sup>Np and <sup>239</sup>Pu. UO<sub>2</sub> was supplied by Westinghouse Atom AB, NpO<sub>2</sub> and PuO<sub>2</sub> were used from Institute for Transuranium Elements (ITU) stocks. Before the start of the experiments the actinide powders were characterized with scanning electron microscope (SEM) to determine the particle size.

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Experiments using  $\text{NpO}_2$  and  $\text{PuO}_2$  were performed in a double glovebox arrangement. Oxygen levels were stabilised in the inner glove box in the range of 1–2 ppm. Experiments measuring  $\text{H}_2\text{O}_2$  consumption using  $\text{UO}_2$  were not performed in a glovebox, instead continuous  $\text{N}_2$  purging was used to ensure low  $\text{O}_2$  levels. The  $\text{UO}_2$  dissolution was measured in separate experiments performed in a glovebox with oxygen levels <0.1 ppm. Actinide oxide powder (30 mg) was mixed with ~20 mM aqueous  $\text{H}_2\text{O}_2$  solution in a glass vessel. The solution volume was 100 ml in the experiments using  $\text{NpO}_2$  and  $\text{PuO}_2$  and 20 ml in the case of  $\text{UO}_2$ . Samples (5 ml) were taken in several time intervals after the start of the experiment.

In the experiments performed using  $\text{NpO}_2$  and  $\text{PuO}_2$ , one portion of the sample was used for determination of the  $\text{H}_2\text{O}_2$  concentration using by UV/visible spectroscopy (Lovibond PCCheckit photometer) at 528 nm using DPD (*N,N*-diethyl-1,4-phenylene diammoniumsulfate as reagent according to the method described in Refs. [7,8]. Another portion was used for determination of the concentration of dissolved actinide. This was performed by inductively coupled plasma mass spectrometry (ICP-MS). This aliquot was passed through 30 kDa MWCO ultrafilters to remove the colloids from the solution. At the end of the experiments the oxidation state distribution in the aqueous phase was analyzed. This was done by oxidation state separation by solvent extraction using the n-octyltrifluoroacetone (TTA) in the case of Pu and DBM (dibenzoylmethane) in the case of Np according to the method described in Refs. [9,10], followed by ICP-MS analysis. The equipment used for ICP-MS was a ThermoFinnigan Element 2 (ThermoFinnigan, Bremen, Germany) installed in a glovebox.

In the experiments performed using  $\text{UO}_2$ , the  $\text{H}_2\text{O}_2$  concentration was measured indirectly by UV/visible spectroscopy (S2000 spectrophotometer from WPA) at 360 nm using  $\text{I}_3^-$  as an indicator. Detailed information about this method can be found in Refs. [11–13]. The concentration of U(VI) in solution was measured by UV/vis spectroscopy at 653 nm using the Arsenazo(III) reagent ( $\epsilon_{653} = 63,000$ ). Detailed information about this method is found in Refs. [14,15].

In order to remove surface fines and establish a uniform oxidation state (remove pre-oxidized U(VI)) the solid uranium dioxide samples were washed three times with 10 mL and 10 mM  $\text{HCO}_3^-$  and three times with pure  $\text{H}_2\text{O}$  prior to the experiment with  $\text{H}_2\text{O}_2$ . The surfaces of neptunium and plutonium were not specially treated before the experiments due to the higher stability of their +IV oxidation states, as confirmed by XPS results.

Due to the different specific activities of the actinide oxides [16], the background levels of radiolytically produced  $\text{H}_2\text{O}_2$  will vary. In order to account for this, background studies were per-

**Table 1**

Initial  $\text{H}_2\text{O}_2$  consumption rates, initial actinide release rates and one-electron reduction potential for the  $\text{AnO}_2^+/\text{An}^{4+}$  [16].

	$d\text{H}_2\text{O}_2/dt$ ( $\text{mol dm}^{-3} \text{s}^{-1}$ )	$E^0$ (mV)	An release rate ( $\text{mol dm}^{-3} \text{s}^{-1}$ )
$\text{UO}_2$	$12 \times 10^{-7}$	380	$2.5 \times 10^{-7}$
$\text{NpO}_2$	$0.9 \times 10^{-7}$	640	$1.5 \times 10^{-11}$
$\text{PuO}_2$	$0.28 \times 10^{-7}$	1040	$4.0 \times 10^{-13}$

formed for  $^{237}\text{Np}$  and  $^{239}\text{Pu}$  where the solution consisted of deionised water.

The uncertainty in the concentration measurements is estimated to ~10%.

### 3. Results and discussion

Using the present data on  $\text{H}_2\text{O}_2$  concentration as a function of reaction time, it is possible to determine the relative rates of  $\text{H}_2\text{O}_2$  induced oxidative dissolution for  $\text{UO}_2$ ,  $\text{NpO}_2$  and  $\text{PuO}_2$ . It should be kept in mind that the rate of  $\text{H}_2\text{O}_2$  consumption does not necessarily reflect only the relative rate constant for oxidation of the actinide oxide. As the experiments have been performed utilizing aqueous solutions free from potential complexing agents, such as  $\text{HCO}_3^-$ , the kinetics for  $\text{H}_2\text{O}_2$  consumption is largely limited by dissolution of the oxidized actinide oxide rather than the redox process [17]. For low conversions, a steady-state approach can be used where the rate of oxidation is identical to the rate of dissolution.

In Fig. 1, the  $\text{H}_2\text{O}_2$  concentration is plotted versus time for the three different actinide oxides. In Table 1, the initial  $\text{H}_2\text{O}_2$  consumption rates are shown.

As can be seen, the initial rate of  $\text{H}_2\text{O}_2$  consumption is highest for  $\text{UO}_2$  followed by  $\text{NpO}_2$  and lowest rate is measured for  $\text{PuO}_2$ . When measuring the  $\text{H}_2\text{O}_2$  consumption, the available surface area of the oxide to solution volume ratio is a critical parameter. The presented results are based on the assumption that the solid surface area to solution volume ratio is equal in the three experiments. Judging from SEM pictures of the materials, the surface area of the  $\text{UO}_2$  powder was estimated to be significantly smaller than for the other materials. In order to obtain similar solid surface area to solution volume ratios, the solution volume was decreased by a factor of five in the experiment using  $\text{UO}_2$ . No compensation has been made for the difference between  $\text{NpO}_2$  and  $\text{PuO}_2$ . This is probably an underestimation of the differences in surface area between the materials; hence the trend in  $\text{H}_2\text{O}_2$  consumption could be even more pronounced than shown here. Interestingly,

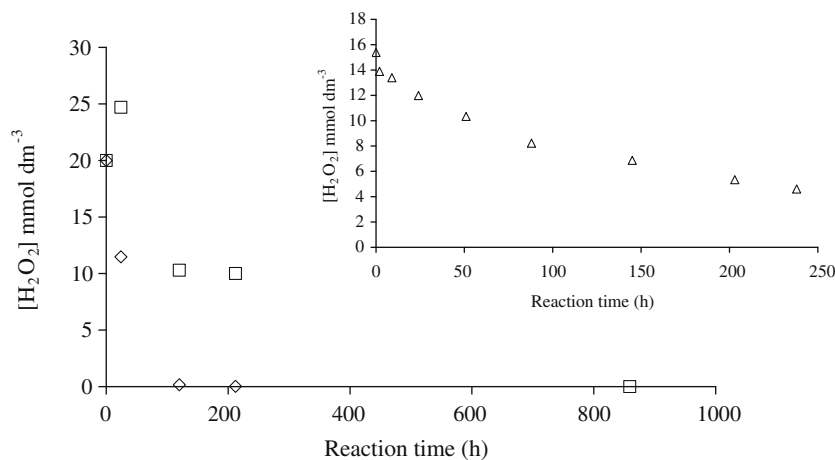


Fig. 1.  $\text{H}_2\text{O}_2$  concentration as a function of reaction time for ( $\Delta$ )  $\text{UO}_2$ , ( $\square$ )  $\text{PuO}_2$  and ( $\diamond$ )  $\text{NpO}_2$ .

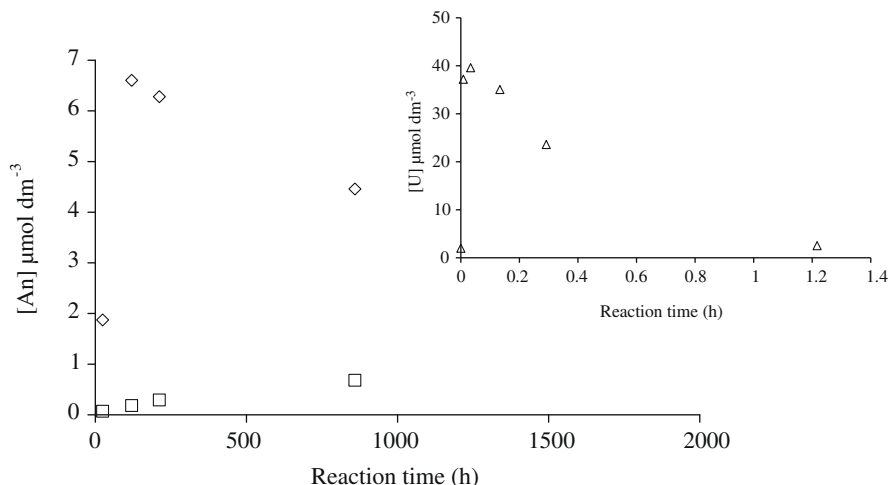


Fig. 2. Dissolved actinide concentration as a function of reaction time for ( $\Delta$ )  $\text{UO}_2$ , ( $\square$ )  $\text{PuO}_2$  and ( $\diamond$ )  $\text{NpO}_2$ .

**Table 2**  
Fraction of oxidized (oxidation state V and VI) actinide in solution at the end of the experiment, based on concentration of oxidized actinide (oxidation state V and VI) and total actinide concentration in solution.

	Background experiment			Experiment with added $\text{H}_2\text{O}_2$		
	Oxidized concentration ( $\mu\text{mol dm}^{-3}$ )	Total concentration ( $\mu\text{mol dm}^{-3}$ )	Oxidized fraction	Oxidized concentration ( $\mu\text{mol dm}^{-3}$ )	Total concentration ( $\mu\text{mol dm}^{-3}$ )	Oxidized fraction
$\text{NpO}_2$	3.3	8.1	0.41	4.1	4.4	0.93
$\text{PuO}_2$	0.09	0.12	0.78	0.7	0.68	1.03

the relative trend in reactivity towards  $\text{H}_2\text{O}_2$  parallels the trend in oxidation potential for the three oxides ( $\text{UO}_2$  has the lowest potential while  $\text{PuO}_2$  has the highest potential [16]).

The observed trend in  $\text{H}_2\text{O}_2$  consumption is qualitatively confirmed by the initial rate of actinide release (Table 1, Fig. 2). In the initial phase of the experiments the actinide concentration increases with increasing reaction time in all three cases. At longer reaction times the concentration of U and Np decreases, whereas the Pu concentration continues to increase. This can probably be attributed to the larger propensity of U and Np to form stable solid peroxide complexes [18,19]. Furthermore, the concentration of dissolved Pu is comparatively low, which limits the formation of the peroxide complex.

It should also be noted that, while the redox reactivity of the actinide oxides towards  $\text{H}_2\text{O}_2$  is expected to depend on the redox potential of the actinide oxide, the rate of surface catalyzed decomposition of  $\text{H}_2\text{O}_2$  is expected to be independent of the redox properties and therefore similar for all three oxides, as previously observed for other metal oxides [17,20–22]. Hence, the impact of the catalytic decomposition route (on the overall  $\text{H}_2\text{O}_2$  decomposition) is expected to increase in the order  $\text{UO}_2 < \text{NpO}_2 < \text{PuO}_2$ . As a direct consequence, the oxidative dissolution yield is expected to decrease in the order  $\text{UO}_2 > \text{NpO}_2 > \text{PuO}_2$ .

The background experiments where no  $\text{H}_2\text{O}_2$  was added revealed very low U release rate. The Pu background release rate was around 15% of the release rate in the  $\text{H}_2\text{O}_2$  experiment. In the Np case the background release rate is approximately 10% of the initial release rate in the  $\text{H}_2\text{O}_2$  experiment. However, since the Np concentration is decreasing at longer times in the presence of  $\text{H}_2\text{O}_2$ , the background concentration will, with time, exceed the Np concentration in the  $\text{H}_2\text{O}_2$  experiment.

When analyzing the distribution of oxidation states in the dissolved Np and Pu at the end of the experiments performed in the presence of  $\text{H}_2\text{O}_2$  and in the background experiments, it was found

that  $\text{H}_2\text{O}_2$  addition increased the fraction of oxidized material. The distribution of oxidation states is presented in Table 2.

This finding indicates that an oxidation reaction is indeed involved in the dissolution mechanism.

$\text{H}_2\text{O}_2$  produced by  $\text{NpO}_2$  under the test conditions was below the detection limit of  $1 \mu\text{M}$  during the whole experiment (35 days). The  $\text{H}_2\text{O}_2$  produced by  $^{239}\text{PuO}_2$  was found to be negligible compared to the amount of added  $\text{H}_2\text{O}_2$ . Decomposition of  $\text{H}_2\text{O}_2$  caused by test conditions (i.e. vessel, atmosphere, surrounding light) was measured to be negligible in the concentrations used.

In conclusion, we have found that oxidative dissolution takes place for all three actinides in the presence of  $\text{H}_2\text{O}_2$  and that the trend in dissolution rate parallels the trend in redox potential of the oxides. However, from the present data we can not draw any conclusions regarding the individual trends for the oxidation and dissolution mechanisms, respectively. In order to gain information on a mechanistic level, experiments with excess of solid material and varying surface to solution volume ratio are needed. Furthermore, the use of a complexing agent would be necessary in order to determine the true rate and rate constant of oxidation without influence of dissolution of oxidized species from the surface.

Based on the dissolution rates obtained in this work, we would not expect the dissolution of the actinides to be congruent. Instead, in a system without complexing agent, the release rates for Np and Pu are expected to be lower than the U release rate. However, in the presence of complexing agents and in systems where the oxides occur in mixed phases these dissolution rates may not be applicable.

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## References

- [1] D.W. Shoesmith, *J. Nucl. Mater.* 282 (2000) 1–31.
- [2] R.L. Segall, R.S.C. Smart, P.S. Turner, Oxide surfaces in solution, in: J. Nowotny, L.-C. Dufour (Eds.), *Surface and Near-Surface Chemistry of Oxide Materials*, Elsevier Science Publishers BV, Amsterdam, 1988, pp. 527–576.
- [3] M. Jonsson, F. Nielsen, O. Roth, E. Ekeröth, S. Nilsson, M.M. Hossain, *Environ. Sci. Technol.* 41 (2007) 7087–7093.
- [4] E.C. Buck, B.D. Hanson, B.K. McNamara, *Energy, Waste Environ.: Geochem Persp* (2004) 65–88 (Geological Society Special Publication 236).
- [5] O. Roth, M. Jonsson, *Cent. Eur. J. Chem.* 6 (2008) 1–14.
- [6] E. Ekeröth, O. Roth, M. Jonsson, *J. Nucl. Mater.* 355 (2006) 38–46.
- [7] H. Bader, V. Sturzenegger, J. Hoigne, *Water Res.* 22 (1988) 1109–1115.
- [8] M. Amme, J. Svedkauskaitė, W. Bors, M. Murray, J. Merino, *Radiochim. Acta* 95 (2007) 683–692.
- [9] J.A. Schramke, R. Dīanpat, R.W. Fulton, G.R. Choppin, *J. Radioanal. Nucl. Chem.* 130 (1989) 333–346.
- [10] P.A. Bertrand, G.A. Choppin, *Radiochim. Acta* 31 (1982) 135–137.
- [11] W.A. Patrick, H.B. Wagner, *Anal. Chem.* 21 (1949) 1279–1280.
- [12] T.C.J. Ovenston, W.T. Rees, *Analyst* 75 (1950) 204–208.
- [13] Y. Nimura, K. Itagaki, K. Nanba, *Nippon Suisan Gakk.* 58 (1992) 1129–1137.
- [14] I.K. Kressin, *Anal. Chem.* 56 (1984) 2269–2271.
- [15] S.B. Savvin, *Talanta* 8 (1961) 673–685.
- [16] J. Katz, G. Seaborg, L. Morss, *The Chemistry of the Actinide Elements*, vol. 2, second ed., Chapman and Hall, London, 1986.
- [17] M.M. Hossain, E. Ekeröth, M. Jonsson, *J. Nucl. Mater.* 358 (2006) 202–208.
- [18] C. Musikas, *Radiochem. Radioanal. Lett.* 7 (1971) 375–379.
- [19] R.F. Leininger, J.P. Hunt, D.E. Koshland Jr., *Composition and Thermal Decomposition of Uranyl Peroxide*, US Atom. Energy Commun., 1958, TID-5290 (Book 2), pp. 704–21.
- [20] E. Ekeröth, M. Jonsson, *J. Nucl. Mater.* 322 (2003) 242–248.
- [21] M.A. Nejad, M. Jonsson, *J. Nucl. Mater.* 334 (2004) 28–34.
- [22] A. Hiroki, J.A. LaVerne, *J. Phys. Chem. B* 109 (2005) 3364–3370.